

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

Claim 1 (Currently Amended) Catalyst A catalyst comprising at least one ZBM-30 (molecular sieve) zeolite synthesized with a particular structuring agent such as consisting essentially of triethylenetetramine, at least one hydro-dehydrogenating element, and at least one porous mineral matrix.

Claim 2 (Currently Amended) Catalyst A catalyst according to claim 1 in which the hydro-dehydrogenating element is chosen from comprises at least one of the elements of Group VIB and Group VIII of the periodic table.

Claim 3 (Currently Amended) Catalyst A catalyst according to claim 2 in which the hydro-dehydrogenating element of Group VIB is comprises molybdenum and/or tungsten.

Claim 4 (Currently Amended) Catalyst A catalyst according to claim 1 in which the hydro-dehydrogenating element of Group VIII is comprises a noble metal of Group VIII.

Claim 5 (Currently Amended) Catalyst A catalyst according to claim 4 in which the hydro-dehydrogenating element of Group VIII is comprises platinum and/or palladium.

Claim 6 (Currently Amended) Catalyst A catalyst according to claim 1 subjected to sulphurization treatment.

Claim 7 (Currently Amended) Process A process for improving the pour point of a paraffin charge, in which the charge to be treated is brought into contact with a dewaxing catalyst comprising at least one ZBM-30 (molecular sieve) zeolite synthesized with a particular structuring agent such as

~~triethylenetetramine, comprising a catalyst according to claim 1, at least one hydro-dehydrogenating, element and at least one porous matrix.~~

Claim 8 (Currently Amended) Process A process according to claim 7 in which the treated charges contain at least 20% by volume of compounds boiling above 340°C.

Claim 9 (Currently Amended) Process A process according to claim 7 in which the operating conditions are the following:

- the reaction temperature is between 200 and 450°C,
- the pressure is between 0.1 and 25 MPa,
- the hourly volume rate (hvr expressed as volume of charge injected per volume unit of catalyst per hour) is between approximately 0.05 and approximately 30h⁻¹.

Claim 10 (Currently Amended) Process A process according to claim 7 in which the charge undergoes a hydroisomerization-hydroconversion stage beforehand.

Claim 11 (Currently Amended) Process A process according to claim 10 in which all of the effluent from the hydroisomerization-conversion stage is sent to the dewaxing catalyst.

Claim 12 (Currently Amended) Process A process according to claim 10 in which the hydroisomerization-hydroconversion stage is preceded by a hydrorefining stage.

Claim 13 (Currently Amended) Process A process according to claim 12 in which the hydrorefining stage is followed by an intermediate separation.

Claim 14 (Currently Amended) Process A process according to claim 7 in which the effluent from the catalytic hydrodewaxing stage is at least partly sent to a hydrofinishing catalyst.

Claim 15 (New) A catalyst according to claim 1, wherein the at least one porous mineral matrix is an amorphous or poorly crystallizable oxide.

Claim 16 (New) A catalyst according to claim 1, wherein the hydro-dehydrogenating agent comprises platinum and the at least one porous mineral matrix comprises alumina.